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PTO/SB/05 (1/98)

UTILITY
PATENT APPLICATION
TRANSMITTAL

(Only for new nonprovisional applications under 37 CFR 1.53(b))

Attorney Docket No. VX961463A PCT

First Named Inventor or Application Identifier Takayuki Araki

Title AQUEOUS DISPERSION OF VINYLIDENE FLUORIDE
POLYMER AND PREPARATION PROCESS THEREOF

Express Mail Label No.

APPLICATION ELEMENTS

See MPEP chapter 600 concerning utility patent application contents.

ADDRESS TO: Assistant Commissioner for Patents
Box Patent Application
Washington, DC 202311. ☒ Fee Transmittal Form (e.g., PTO/SB/17)
(Submit an original, and a duplicate for fee processing)2. ☒ Specification [Total Pages 16]
(preferred arrangement set forth below)

- Descriptive title of the Invention
- Cross References to Related Applications
- Statement Regarding Fed sponsored R & D
- Reference to Microfiche Appendix
- Background of the Invention
- Brief Summary of the Invention
- Brief Description of the Drawings (if filed)
- Detailed Description
- Claim(s)
- Abstract of the Disclosure

3. ☐ Drawing(s) (35 USC 113) [Total Sheets ☐

4. Oath or Declaration [Total Pages 16]

- a. ☐ Newly executed (original or copy)
- b. ☒ Copy from a prior application (37 CFR 1.63(d))
(for continuation/divisional with Box 17 completed)
[Note Box 5 below]

i. ☐ DELETION OF INVENTOR(S)
Signed statement attached deleting
inventor(s) named in the prior application,
see 37 CFR 1.63(d)(2) and 1.33(b).5. ☒ Incorporation By Reference (useable if Box 4b is checked)
The entire disclosure of the prior application, from which a
copy of the oath or declaration is supplied under Box 4b
is considered as being part of the disclosure of the
accompanying and is hereby incorporated by
reference therein.6. ☐ Microfiche Computer Program (Appendix)7. Nucleotide and/or Amino Acid Sequence Submission
(if applicable, all necessary)

- a. ☐ Computer Readable Copy
- b. ☐ Paper Copy (identical to computer copy)
- c. ☐ Statement verifying identity of above copies

ACCOMPANYING APPLICATION PARTS

- 8. ☐ Assignment Papers (cover sheet & document(s))
- 9. ☐ 37 CFR 3.73(b) Statement ☐ Power of Attorney
(when there is an assignee)
- 10. ☐ English Translation Document (if applicable)
- 11. ☒ Information Disclosure ☐ Copies of IDS
Statement (IDS)/PTO -1449 Citations
- 12. ☒ Preliminary Amendment
- 13. ☐ Return Receipt Postcard (MPEP 503)
(Should be specifically itemized)
- 14. ☐ Small Entity ☐ Statement filed in prior application
Statement(s) Status still proper and desired
- 15. ☐ Certified Copy of Priority Document(s)
(if foreign priority is claimed)
- 16. ☐ Other:

*A new statement is required to be entitled to pay small entity fees, except where one
has been filed in a prior application and is being relied upon.

17. If a CONTINUING APPLICATION, check appropriate box, and supply the requisite information below and in a preliminary amendment:

☒ Continuation ☐ Divisional ☐ Continuation-in-part (CIP) of prior application No: 08/612,865

Prior application information. Examiner: Peter Szekely

Group/Art Unit: 1511

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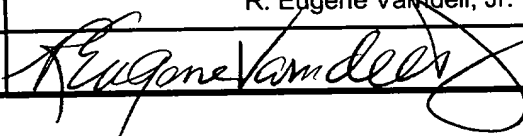
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Date

6/11/98

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22-0256

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

In re the application of:

Takayuki Araki *et al.*

Prior Appln.

Serial Number: Cont. Appln. of 08/612,865

Art Group Unit: 1511

Filed: June 11, 1998 (herewith)

Examiner: Peter Szekely

For: AQUEOUS DISPERSION OF VINYLIDENE FLUORIDE POLYMER AND
PREPARATION PROCESS THEREOF

PRELIMINARY AMENDMENT

Honorable Commissioner
of Patents and Trademarks
Washington, D.C. 20231

June 11, 1998

Dear Sir:

Prior to an examination on the merits, please amend the above-identified
application as follows:

IN THE SPECIFICATION:

Page 2, line 21, change "anion" --anionic--.

Page 2, line 22, change "nonion" --nonanionic--.

IN THE CLAIMS:

Claim 1, line 3, change "a" --an average--.

Claim 3, line 3, delete "or 2".

Please cancel Claim 2 and add the following new claims:

--4. The aqueous dispersion of a vinylidene fluoride polymer of Claim 1, wherein the nonionic non-fluorine-containing surfactant is a polyoxyethylene alkyl ether or a polyoxyethylene alkyl ester.

5. The process of Claim 3, wherein nonionic non-fluorine-containing surfactant is a polyoxyethylene alkyl ether or a polyoxyethylene alkyl ester.--

REMARKS

Applicants' specification has been amended to correct typographical errors. Claim 1 has been amended to define an average particle size, which is described in applicants' specification disclosure at, for example, page 10, lines 4-11. Claim 2 has been canceled. Claims 4 and 5 have been added to the application which define specific non-fluorine-containing surfactants, such as those described on pages 6 and 7 of applicants' specification disclosure, especially at the page 7, lines 27-33. Accordingly, Claims 1 and 3 to 5 are in the application for consideration by the Examiner.

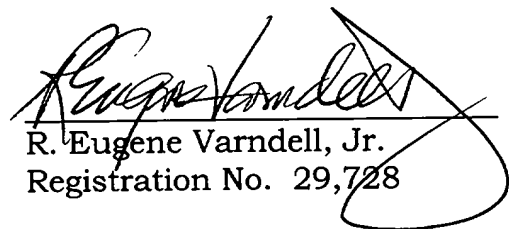
In the most recent Office Action in the parent application, no prior art rejections were set forth. Two rejections of Claim 1 were set forth, one under 35 U.S.C. § 112, first paragraph, and the second under 35 U.S.C. § 112, second paragraph. In the rejection under 35 U.S.C. § 112, first paragraph, it was stated that the specification does not enable a person skilled in the art to which it pertains or with which it is most nearly connected to make the invention commensurate in scope with the claims. The Official Action noted

page 6, lines 28-37, as describing that in order to decrease the concentration of the fluorinated surfactant to not more than 1%, a trace amount of non-fluorine-containing surfactant has to be added. Applicant respectfully submits that the positions concerning the description on page 6, lines 29-37, of the present specification are incorrect. In particular, applicant respectfully submits that there is no absolute requirement for the presence of the non-fluorine-containing surfactant at this portion of applicant's specification. In other words, applicant respectfully submits that this portion of this specification does not require the presence of the non-fluorine-containing surfactant in applicant's invention. This portion of applicant's specification disclosure simply states that it is possible to decrease the amount of fluorine-containing surfactant to a smaller amount of not more than 1% by weight by adding a trace amount of the non-ionic non-fluorine-containing surfactant. This portion of applicant's specification disclosure does not state that it is not possible to decrease the amount of fluorine-containing surfactant in another way. Accordingly, it is respectfully submitted that applicant's specification disclosure would enable any person skilled in the art to make the invention as set forth in Claim 1 within the meaning of the first paragraph of 35 U.S.C. § 112, and further, that Claim 1 particularly points out and distinctly claims applicant's invention within the meaning the second paragraph of 35 U.S.C. § 112.

It is respectfully noted that Comparative Example 5, which does not include the use of a non-ionic non-fluorine-containing surfactant provides an average particle size of not more than 200 nm, is within the scope of Claim 1. Accordingly, this example demonstrates that the particle sizes of applicant's claims can be obtained without the use of the non-fluorine-containing surfactant, thereby enabling the invention claimed in Claim 1. This example further demonstrates at the time of invention the applicant had within its possession a composition as set forth in Claim 1, namely, one without any nonionic non-fluorine-containing surfactant.

For the foregoing reasons, applicant respectfully submits that the claims of the present application comply with both the first and second paragraphs of 35 U.S.C. § 112. Therefore, early consideration and allowance of Claims 1 and 3 through 5 are respectfully requested.

Respectfully submitted,
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DESCRIPTION

AQUEOUS DISPERSION OF VINYLIDENE FLUORIDE POLYMER AND PREPARATION PROCESS THEREOF

5

TECHNICAL FIELD

The present invention relates to an aqueous dispersion of a fluorine-containing polymer usable for
10 paints. More specifically the present invention relates to an aqueous dispersion of a vinylidene fluoride (VdF) type polymer, which comprises a VdF polymer having a particle size of not more than 200 nm and contains 30 to 50 % by weight of solids, and a process for preparation
15 thereof.

BACKGROUND ART

Fluorine-containing paints are used as weather resistive paints for exterior and interior coating of
20 medium- or low-storied buildings, and various techniques have been developed for preparation of the fluorine-containing paints. Though many of the fluorine-containing paints are in the form of organic solvent dispersions, there are problems in the use of organic solvents from
25 safety and environmental protection points of view, and ones of aqueous dispersion type are preferable. As the methods of preparing an aqueous dispersion of a fluorine-containing polymer, there are known the methods mentioned below.

30 For example, JP-B-28669/1974 discloses that when vinyl fluoride is suspension-polymerized in preparation of paints, a nonionic surfactant is added in an amount of 0.05 to 5 % by weight on the basis of the monomer to increase yield, to prevent deposition of the polymer onto
35 an inside wall of a polymerization tank and to control particle size of the polymer.

Also JP-A-123646/1986 discloses that in preparing a fluorine-containing copolymer in an aqueous

medium, a stable aqueous emulsion can be obtained by adding a dispersion stabilizing agent after polymerization of the fluorine-containing copolymer, but before or during the condensation process of the aqueous dispersion.

5 Further JP-B-55441/1992 discloses that in preparing an aqueous fluorine-containing polymer dispersion for aqueous paints, 0.05 to 5.0 % by weight of surfactants of various kinds including a nonionic surfactant is added when the seed-polymerization of a
10 monomer having ethylenically unsaturated bond is carried out.

Also JP-A-225550/1990 discloses that a mixture of a fluorine-containing type surfactant and a nonionic type surfactant is used when copolymerizing a
15 fluorine-containing olefin and a hydrophilic group-containing non-fluorine-containing olefin.

Also Koubunshi Ronbun Shu, Vol. 36, No. 11 (1979) discloses at pages 729 to 737 that when a large amount of surfactants of various kinds is used in emulsion
20 polymerization, particles of a polymer latex become smaller, and also that by mixing an anion surfactant and a nonion surfactant in polymerization of an acrylic monomer, there can be obtained the same effect as in case of adding an anion surfactant solely.

25 However the technique in JP-B-28669/1974 does not relate to emulsion polymerization, but relates to suspension polymerization without using a fluorine-containing surfactant, and intends to obtain a particle size larger than that of the present invention.
30 The particle size described in Example of this patent publication is as large as 3.4 to 4.5 μm .

Also JP-A-123646/1986 discloses that a polymer latex having a concentration as high as not less than 30 % by weight is obtained by using a fluorine-containing
35 emulsifying agent in polymerization process. However there is no description as to the use of a fluorine-containing surfactant for controlling the particles at a size lower than a certain size. In

addition, the invention is characterized by the use of a specific non-fluorine-containing dispersion stabilizing agent, and its amount to be used is as much as 2 to 8 % by weight on the basis of a solid content. Usually the
5 particle size of a latex tends to increase together with a polymer concentration, and when the fluorine-containing surfactant is used solely and if its amount is not more than 1 % by weight, there cannot be obtained a particle size of not more than 200 nm if the solid content is
10 assumed to be 30 to 50 % by weight. Also there is no description as to controlling of the particle size of the aqueous latex. It is also described that if the nonionic surfactant is added in preparing an aqueous emulsion, there is an adverse effect such as coloring.

15 Further in the technique disclosed in JP-B-55441/1992, no surfactant is used in the polymerization of a fluorine-containing olefin, and also there is no disclosure as to the use of a fluorine-containing surfactant as the surfactant to be
20 used in the seed-polymerization.

Also the technique specifically disclosed in JP-A-225550/1990 is one wherein chlorotrifluoroethylene is used as a fluoroolefin unit and the amount of the nonionic surfactant used is as relatively much as 3 % by weight on
25 the basis of water. However in copolymerization of VdF, there has been generally known that there occur problems such that when the nonionic surfactant is added, the reaction rate is lowered remarkably and the molecular weight is not increased.

30 Also in the techniques disclosed in the above-mentioned Koubunshi Ronbun Shu, the use of the surfactant in a large amount causes an adverse effect on water resistance when used for paints.

The present invention has been made to solve the
35 above-mentioned problems, and it is an object of the present invention to provide an aqueous dispersion of a fluorine-containing polymer, which comprises a VdF polymer having a particle size as small as not more than 200 nm

and contains solids in an amount as high as 30 to 50 % by weight and a surfactant in an amount as low as not more than 1 % by weight on the basis of water, and its preparation process.

5

DISCLOSURE OF THE INVENTION

The present invention relates to an aqueous dispersion of a VdF polymer, which comprises a VdF polymer having a particle size of not more than 200 nm, has a
10 solid content of 30 to 50 % by weight and contains a fluorine-containing surfactant in an amount of not more than 1 % by weight on the basis of water.

It is possible in the present invention that in the known emulsion polymerization system, notwithstanding
15 that the solid content is as high as 30 to 50 % by weight, the particle size can be decreased to not more than 200 nm by adding a nonionic non-fluorine-containing surfactant in a trace amount of 0.001 to 0.1 % by weight on the basis of water in the presence of a small amount of a
20 fluorine-containing surfactant, i.e. not more than 1 % by weight, on the basis of water.

BEST MODE FOR CARRYING OUT THE INVENTION

As the VdF polymer in the present invention,
25 there are homopolymer of VdF; a copolymer of VdF monomer and at least one of the other fluorine-containing monomers such as tetrafluoroethylene (TFE), trifluoroethylene (TrFE), chlorotrifluoroethylene (CTFE) and hexafluoropropylene (HFP); a copolymer of VdF, the other
30 fluorine-containing monomer and a monomer having an unsaturated bond which is copolymerizable therewith. The preferable copolymers are, for example, VdF/TFE copolymer, VdF/TFE/HFP copolymer, VdF/TFE/CTFE copolymer, VdF/TFE/TrFE copolymer, VdF/CTFE copolymer, VdF/HFP
35 copolymer, VdF/TFE/HFP/CTFE copolymer, VdF/TFE/perfluorobutenoic acid copolymer, VdF/TFE/maleic acid copolymer and the like. The content of VdF units of these copolymers is preferably not less than 50 % by mole,

more preferably not less than 70 % by mole. The weight average molecular weight (Mw) of these VdF polymers is from 1,000 to 1,000,000, preferably from 10,000 to 500,000. When lower than 1,000, mechanical properties and weatherability when forming a film tend to be inferior, and when higher than 1,000,000, there are tendencies that the resin does not flow when forming a film, leveling property is lowered and no gloss is exhibited.

The particle size of the VdF polymer is not more than 200 nm, preferably from 150 to 100 nm. Since the particle size is as small as not more than 200 nm, the polymer is excellent in stability against sedimentation and dispersing property of additives is excellent. When the particle size is larger than 200 nm, there occurs sedimentation and coagulation of the particles during storage of the dispersion and the dispersing property of the additives is poor. Also there is a tendency that gloss of the formed film is difficult to be obtained.

The fluorine-containing surfactant used in the present invention is one or a mixture of compounds containing fluorine atoms in their structures and having surface activity. For example, there are an acid represented by $X(CF_2)_nCOOH$ (n is an integer of 6 to 20, X is F or H), its alkali metal salt, ammonium salt, amine salt or quaternary ammonium salt; an acid represented by $Y(CH_2CF_2)_mCOOH$ (m is an integer of 6 to 13, Y is F or Cl), its alkali metal salt, ammonium salt, amine salt or quaternary ammonium salt; or the like. More specifically there are used an ammonium salt of perfluoro(octanoic acid), an ammonium salt of perfluoro(nonanoic acid) or the like. In addition, there can be used known fluorine-containing surfactants.

The amount of the fluorine-containing surfactant to be used is not more than 1.0 % by weight on the basis of water, preferably not more than 0.5 % by weight, more preferably not more than 0.2 % by weight. The lower limit is usually 0.01 % by weight. When more than 1.0 % by weight, there occurs a phenomenon such as precipitation of

the surfactant in the film formed from the aqueous dispersion and also there is a tendency such that water absorption increases to make the dispersion whiten. Thus it is not preferable if the amount of the
5 fluorine-containing surfactant is more than 1.0 % by weight.

The solid content of the aqueous dispersion of the present invention is from 30 to 50 % by weight, preferably from 35 to 45 % by weight. When less than 30 %
10 by weight, there is a tendency such that when forming a film, viscosity adjustment is difficult and leveling property is lowered. When more than 50 %, stability of the dispersion becomes worse, and deposition and coagulation tend to occur in polymerization process.

15 Water to be used for an aqueous dispersion of the present invention is preferably a deionized water.

The aqueous dispersion of the VdF polymer of the present invention can be prepared, for example, by emulsion-polymerizing VdF monomer or a monomer mixture
20 containing VdF under coexistence of the above-mentioned fluorine-containing surfactant in an amount of not more than 1 % by weight on the basis of water and a trace amount of the nonionic non-fluorine-containing surfactant.

25 In order to prepare the aqueous dispersion which comprises the VdF polymer having a particle size of not more than 200 nm and contains solids in an amount of 30 to 50 % by weight, it is usually necessary to use a large amount of a fluorine-containing surfactant. However
30 according to the preparation process of the present invention, it is possible to decrease the amount of the fluorine-containing surfactant to a small amount of not more than 1 % by weight by adding a trace amount of the nonionic non-fluorine-containing surfactant. Namely, a
35 small particle size of not more than 200 nm can be attained by adding the nonionic non-fluorine-containing surfactant.

As the nonionic non-fluorine-containing

surfactant, there are polyoxyethylene alkyl ethers, polyoxyethylene alkyl phenyl ethers, polyoxyethylene alkyl esters, sorbitan alkyl esters, polyoxyethylene sorbitan alkyl esters, glycerol esters, their derivatives and the like. More specifically examples of polyoxyethylene alkyl ethers are polyoxyethylene lauryl ether, polyoxyethylene cetyl ether, polyoxyethylene stearyl ether, polyoxyethylene oleyl ether, polyoxyethylene behenyl ether and the like; examples of polyoxyethylene alkyl phenyl ethers are polyoxyethylene nonyl phenyl ether, polyoxyethylene octyl phenyl ether and the like; examples of polyoxyethylene alkyl esters are polyethylene glycol monolaurate, polyethylene glycol monooleate, polyethylene glycol monostearate and the like; examples of sorbitan alkyl esters are polyoxyethylene sorbitan monolaurate, polyoxyethylene sorbitan monopalmitate, polyoxyethylene sorbitan monostearate, polyoxyethylene sorbitan monooleate and the like; examples of polyoxyethylene sorbitan alkyl esters are polyoxyethylene sorbitan monolaurate, polyoxyethylene sorbitan monopalmitate, polyoxyethylene sorbitan monostearate and the like; and examples of glycerol esters are glycerol monomyristate, glycerol monostearate, glycerol monooleate and the like. Also examples of their derivatives are polyoxyethylene alkyl amine, polyoxyethylene alkyl phenyl-formaldehyde condensate, polyoxyethylene alkyl ether phosphate and the like. Particularly preferable are polyoxyethylene alkyl ethers and polyoxyethylene alkyl esters which have an HLB value of 10 to 18. More particularly there are polyoxyethylene lauryl ether (EO: 5 to 20. EO stands for an ethylene oxide unit.), polyethylene glycol monostearate (EO: 10 to 55) and polyethylene glycol monooleate (EO: 6 to 10).

The amount of the nonionic non-fluorine-containing surfactant used in the present invention is from 0.001 to 0.1 % by weight on the basis of water, preferably from 0.01 to 0.05 % by weight. When more than 0.1 % by weight, it is not practicable because the rate of

reaction is lowered because of chain transfer reaction and the reaction is stopped. Also when less than 0.001 % by weight, there is almost no effect of making the particle size fine.

5 The emulsion having a relatively high concentration can also be obtained by polymerizing, in an organic solvent, a monomer mixture containing an ethylenically unsaturated monomer having an ionic group or polyalkylene oxide group, then adding water and distilling
10 off the organic solvent. For example, an emulsion can be obtained by solution-polymerizing, in ethyl acetate, a mixture of VdF, TFE and perfluorobutenoic acid ($\text{CF}_2=\text{CF}-\text{CF}_2\text{COOH}$), adding aqueous ammonia solution to neutralize, then pouring dropwise into ion-exchanged water
15 containing a fluorine-containing surfactant with stirring to disperse homogeneously, and distilling off ethyl acetate by using an evaporator.

 In order to polymerize VdF monomer, an initiator is usually used. As the initiator, particularly there is
20 no restriction if it serves to generate radicals usable for free radical reaction in an aqueous medium at a temperature between 20°C and 90°C. Usually as the water soluble initiator, there are potassium salt and ammonium salt of persulfuric acid, and hydrogen peroxide; and as
25 the oil soluble initiator, there are diisopropyl peroxydicarbonate (IPP), azobisisobutyronitrile (AIBN) and the like. The amount of the initiator to be added is from 0.005 to 1.0 % by weight on the basis of water, preferably from 0.01 to 0.5 % by weight. When less than 0.005 % by
30 weight, the polymerization rate tends to be lowered extremely, and when more than 1.0 % by weight, there is a tendency such that a concentration of an electrolyte is increased and thus the particle size is increased.

 In preparing the aqueous dispersion of the VdF
35 polymer of the present invention, the polymerization temperature is from 20° to 120°C, preferably from 30° to 70°C. When lower than 20°C, in general there is a tendency such that stability of the formed latex is

lowered, and when higher than 120°C, the polymerization rate tends to be decreased due to chain transfer reaction. Polymerization is usually carried out by heating for 5 to 100 hours under a pressure of 1.0 to 50 kgf/cm² (gauge pressure) though it depends on kind of the polymer.

The aqueous dispersion of the VdF polymer of the present invention can be used as water base paints for coating by blending additives such as pigments, thickeners, dispersing agents, defoaming agents, antifreezing agents and film forming auxiliaries or in addition thereto by combining with other high molecular compounds.

The present invention is explained further in detail based on examples, but is not limited thereto.

EXAMPLE 1

A one-liter pressure resistive reactor equipped with a stirrer was charged with 500 ml of deionized water, 0.5 g of a fluorine-containing surfactant, i.e. an ammonium salt of perfluoro(octanoic acid) (PFOA) and 0.05 g of a nonionic non-fluorine-containing surfactant, i.e. polyoxyethylene lauryl ether (MYS40 available from Nikko Chemicals Co., Ltd.), and steps of introduction of pressurized nitrogen gas and deaeration were repeated to remove the dissolved air. The inside pressure of the reactor was then raised to 20 kgf/cm² (gauge pressure) at 60°C by using VdF. Then 0.2 g of an initiator, i.e. ammonium persulfate was added, VdF was continuously supplied to maintain the inside pressure of the reactor constant at 20 kgf/cm² (gauge pressure), and the reaction was carried out for 20 hours. Afterwards the reaction system was rendered to normal temperature and normal pressure, and thereby the reaction was terminated. The intrinsic viscosity $[\eta]$ of the obtained polymer comprising VdF solely, which was measured in a dimethylfuran (DMF) solvent at 35°C, was 0.63. The measured characteristic values of the obtained aqueous dispersion are shown in TABLE 1.

In TABLE 1, the solid content is represented in percentage of the weight of the aqueous dispersion after dried at 150°C for one hour in a vacuum dryer to its weight before drying. The particle size is an average size obtained by measuring the particle sizes with a laser beam scattering particle size analyzer (ELS-3000 available from Otsuka Denshi Kogyo Kabushiki Kaisha). The stability against sedimentation was evaluated as follows by allowing an aqueous dispersion to be tested to stand at 25°C for 60 days.

○: There is no change in dispersed state with naked eyes.

△: The dispersion is separated into a transparent water phase and a dispersed particle phase and it is possible to re-disperse by shaking.

×: The dispersion is separated into a transparent water phase and a dispersed particle phase, and it is impossible to re-disperse by shaking.

EXAMPLE 2

A one-liter pressure resistive reactor equipped with a stirrer was charged with 500 ml of deionized water, 0.5 g of an ammonium salt of perfluoro(octanoic acid) and 0.05 g of polyoxyethylene lauryl ether, and steps of introduction of pressurized nitrogen gas and deaeration were repeated to remove the dissolved air. The inside pressure of the reactor was then raised to 8 kgf/cm² (gauge pressure) at 60°C by using a VdF/TFE monomer mixture (80/20 % by mole). Then 0.05 g of ammonium persulfate was added, the above-mentioned monomer mixture was continuously supplied to maintain the inside pressure of the reactor constant at 8 kgf/cm² (gauge pressure), and the reaction was carried out for 20 hours. Afterwards the reaction system was rendered to normal temperature and normal pressure, and thereby the reaction was terminated. The intrinsic viscosity $[\eta]$ of the obtained VdF/TFE

copolymer in a methyl ethyl ketone (MEK) solution at 35°C was 1.43. The measured characteristic values of the obtained aqueous dispersion are shown in TABLE 1.

5

EXAMPLE 3

A one-liter pressure resistive reactor equipped with a stirrer was charged with 500 ml of deionized water, 0.5 g of an ammonium salt of perfluoro(octanoic acid) and 0.05 g of polyoxyethylene lauryl ether, and steps of
10 introduction of pressurized nitrogen gas and deaeration were repeated to remove the dissolved air. The inside pressure of the reactor was then raised to 8 kgf/cm² (gauge pressure) at 60°C by using a VdF/TFE/HFP monomer mixture (72/20/8 % by mole). Then 0.2 g of ammonium
15 persulfate was added, the above-mentioned monomer mixture was continuously supplied to maintain the inside pressure of the reactor constant at 8 kgf/cm² (gauge pressure), and the reaction was carried out for 38 hours. Afterwards the reaction system was rendered to normal temperature and
20 normal pressure, and thereby the reaction was terminated. The intrinsic viscosity $[\eta]$ of the obtained VdF/TFE/HFP copolymer in an MEK solvent at 35°C was 1.08. The measured characteristic values of the obtained aqueous dispersion are shown in TABLE 1.

25

EXAMPLE 4

A one-liter pressure resistive reactor equipped with a stirrer was charged with 500 ml of deionized water, 0.5 g of an ammonium salt of perfluoro(octanoic acid) and
30 0.05 g of polyoxyethylene lauryl ether, and steps of introduction of pressurized nitrogen gas and deaeration were repeated to remove the dissolved air. The inside pressure of the reactor was raised to 8 kgf/cm² (gauge pressure) at 60°C by using a VdF/TFE/CTFE monomer mixture
35 (75/15/10 % by mole). Then 0.2 g of ammonium persulfate was added, the above-mentioned monomer mixture was continuously supplied to maintain the inside pressure of the reactor constant at 8 kgf/cm² (gauge pressure), and

the reaction was carried out for 40 hours. Afterwards the reaction system was rendered to normal temperature and normal pressure, and thereby the reaction was terminated. The intrinsic viscosity $[\eta]$ of the obtained VdF/TFE/CTFE copolymer in an MEK solvent at 35°C was 1.20. The measured characteristic values of the obtained aqueous dispersion are shown in TABLE 1.

COMPARATIVE EXAMPLES 1 TO 4

10 Aqueous dispersions of the VdF polymer were prepared in the same manner as in EXAMPLES 1 to 4 except that the nonionic non-fluorine-containing surfactant was not used and the amount of the fluorine-containing surfactant was changed as shown in TABLE 1. The measured
15 characteristic values of the obtained aqueous dispersions are shown in TABLE 1.

COMPARATIVE EXAMPLE 5

20 An aqueous dispersion of the VdF polymer was prepared in the same manner as in EXAMPLE 3 except that CTFE was used instead of HFP and the amount of the fluorine-containing surfactant was changed as shown in TABLE 1. The measured characteristic values of the obtained aqueous dispersion are shown in TABLE 1. As
25 shown in TABLE 1, these characteristics were preferable, but there was found precipitation of the fluorine-containing surfactant at drying the formed film.

TABLE 1

	Ex. 1	Ex. 2	Ex. 3	Ex. 4	Com. Ex. 1	Com. Ex. 2	Com. Ex. 3	Com. Ex. 4	Com. Ex. 5
Monomer (% by mole)									
VdF*1	100	80	72	75	100	80	72	75	72
TFE*2	-	20	20	15	-	20	20	15	20
HFP*3	-	-	8	-	-	-	8	-	-
CTFE*4	-	-	-	10	-	-	-	10	8
Surfactant (% by weight)									
Fluorine- containing type	PFOA*5 (0.1)	PFOA (0.1)	PFOA (0.1)	PFOA (0.1)	PFOA (1.0)	PFOA (1.0)	PFOA (1.0)	PFOA (0.1)	PFOA (2.0)
Nonionic non-fluorine- containing type	MYS40*6 (0.01)	MYS40 (0.01)	MYS40 (0.01)	MYS40 (0.01)	-	-	-	-	-
Aqueous dispersion									
Solid content (% by weight)	30.1	32.1	33.4	42.0	18.5	24.6	32.0	34.6	31.5
Particle size (nm)	180.5	167.3	125.9	165.0	231.7	269.2	234.5	320.1	196.3
Stability against sedimentation	○	○	○	○	△	×	×	×	○

*1 Vinylidene fluoride

*2 Tetrafluoroethylene

*3 Hexafluoropropylene

*4 Chlorotrifluoroethylene

*5 Ammonium salt of perfluoro(octanoic acid)

*6 Polyoxyethylene lauryl ether available from Nikko Chemicals Co., Ltd.

INDUSTRIAL APPLICABILITY

The aqueous dispersion of the VdF polymer of the present invention is excellent in stability against sedimentation notwithstanding a small amount of a
5 surfactant and can provide coating films excellent in water resistance and leveling property. According to the preparation process of the present invention, the above-mentioned aqueous dispersion can be prepared easily by using a trace amount of a nonionic
10 non-fluorine-containing surfactant even if the amount of a fluorine-containing surfactant is decreased greatly.

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CLAIMS

1. An aqueous dispersion of a vinylidene fluoride polymer, which comprises a vinylidene fluoride polymer having a particle size of not more than 200 nm, wherein a solid content is from 30 to 50 % by weight and a content of a fluorine-containing surfactant is not more than 1 % by weight on the basis of water.
2. The aqueous dispersion of the vinylidene fluoride polymer of Claim 1, which contains 0.001 to 0.1 % by weight of a nonionic non-fluorine-containing surfactant on the basis of water.
3. A process for preparing the aqueous dispersion of the vinylidene fluoride polymer of Claim 1 or 2, wherein vinylidene fluoride monomer or a monomer mixture containing vinylidene fluoride is emulsion-polymerized under coexistence of not more than 1 % by weight of a fluorine-containing surfactant on the basis of water and 0.001 to 0.1 % by weight of a nonionic non-fluorine-containing surfactant on the basis of water.

ABSTRACT

Aqueous dispersion of a vinylidene fluoride (VdF) polymer which comprises a VdF polymer having a particle size of not more than 200 nm and contains 30 to 50 % by weight of solids and not more than 1 % by weight of a fluorine-containing surfactant on the basis of water. This aqueous dispersion is prepared by emulsion-polymerizing VdF monomer or a monomer mixture containing VdF under coexistence of not more than 1 % by weight of the fluorine-containing surfactant and 0.001 to 0.1 % by weight of a nonionic non-fluorine-containing surfactant on the basis of water, and is suitably used for paints.

Declaration for Patent Application

As a below named inventor, I hereby declare that:

My residence, post office address and citizenship are as stated below next to my name.

I believe I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled AQUEOUS DISPERSION OF VINYLIDENE FLUORIDE POLYMER
AND PREPARATION PROCESS THEREOF, the specification of which

(check one) ☐ is attached hereto.

☒ was filed on September 16, 1994 as International
PCT Application Serial No. PCT/JP94/01531
and was amended on _____
(if applicable)

I hereby state that I have reviewed and understand the contents of the above identified application, including the claim(s), as amended by any amendment referred to above.

I acknowledge the duty to disclose information which is material to the examination of this application in accordance with the Title 37, Code of Federal Regulations, §1.56(a).

I hereby claim foreign priority benefits under Title 35, United States Code, §119 of any foreign application(s) for patent or inventor's certificate listed below and have also identified below any foreign application for patent or inventor's certificate having a filing date before that of the application on which priority is claimed:

Prior Foreign Application(s)		Priority Claimed
<u>233858/1993</u> (Number)	<u>Japan</u> (Country)	<u>20/9/1993</u> (Day/Month/Year Filed)
		<input checked="" type="checkbox"/> Yes <input type="checkbox"/> No
<u> </u> (Number)	<u> </u> (Country)	<u> </u> (Day/Month/Year Filed)
		<input type="checkbox"/> Yes <input type="checkbox"/> No
<u> </u> (Number)	<u> </u> (Country)	<u> </u> (Day/Month/Year Filed)
		<input type="checkbox"/> Yes <input type="checkbox"/> No

I hereby claim the benefit under Title 35, United States Code, §120 of any United States application(s) listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States application in the manner provided by the first paragraph of Title 35, United States Code, §112, I acknowledge the duty to disclose material information as defined in Title 37, Code of Federal Regulations, §1.56(a) which occurred between the filing date of the prior application and the national or PCT international filing date of this application:

<u> </u> (Application Serial No.)	<u> </u> (Filing Date)	<u> </u> (Status)(patented, pending, abandoned)
<u> </u> (Application Serial No.)	<u> </u> (Filing Date)	<u> </u> (Status)(patented, pending, abandoned)

And I hereby appoint as principal attorney R. Eugene Varndell, Jr., Reg. No. 29,728.

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I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

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Inventor's signature _____ Date

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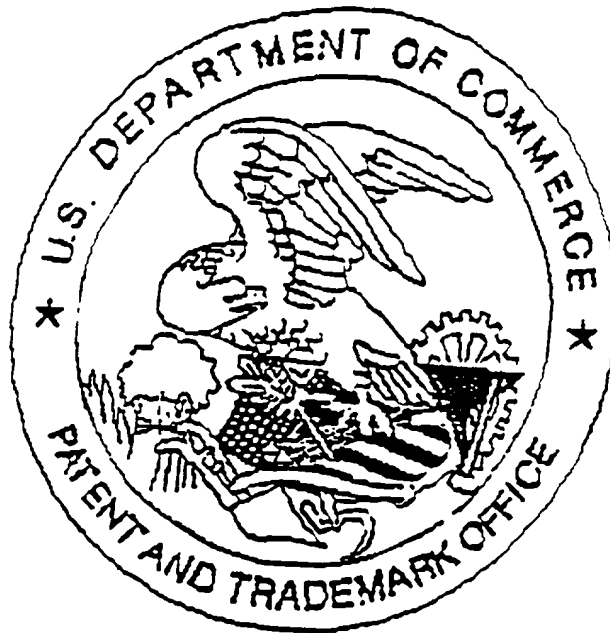
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Inventor's signature _____ Date

Full name of eighth joint inventor _____
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